

RTM製程問題仿真預測及解析

CONFIDENTIAL

Outline

- > **Introduction**
- > **Implementation details**
- > **Case study for Resin Transfer Molding**
- > **Conclusions**
- > **Acknowledge**

Introduction

Moldex3D

Introduction

- > Resin transfer molding(RTM)
 - A branch of a broader class of fiber reinforced composite process known as Liquid Composite Molding (LCM)
 - Different to SRIM (Structural Reaction Injection Molding) for its longer filling time under lower pressures

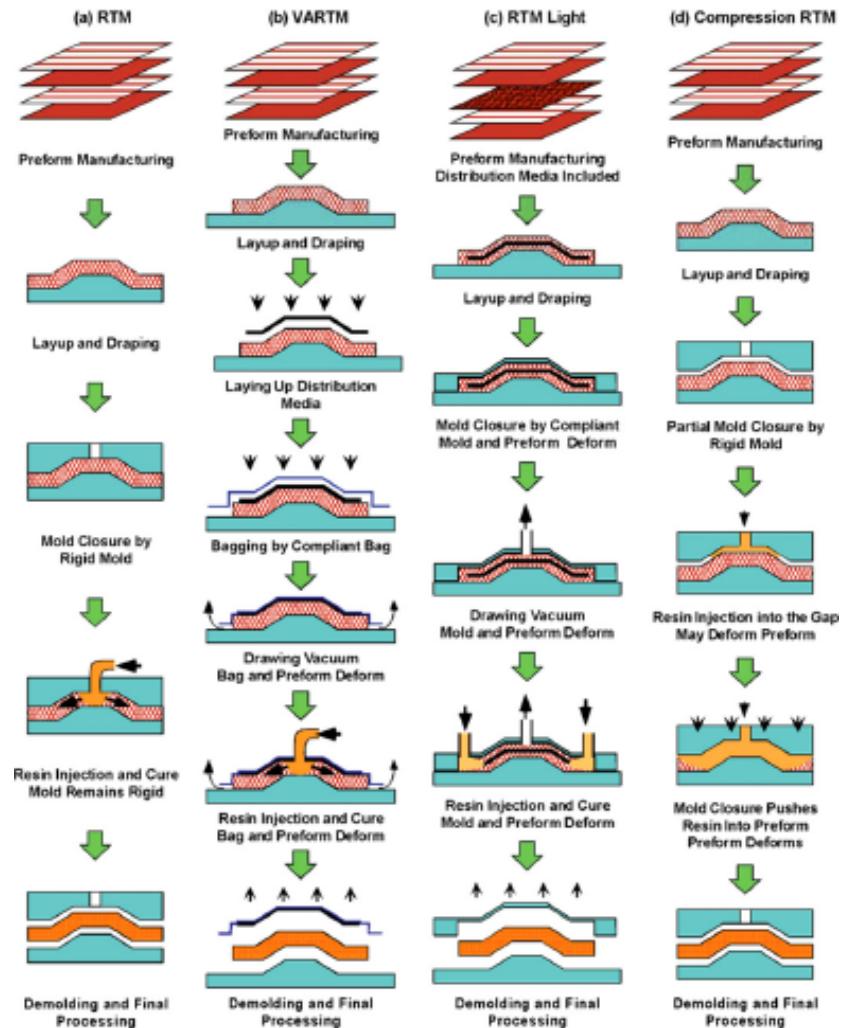


<http://www.swancor.com.tw>

<http://www.moneydj.com/KMDJ/News/>

Introduction

- > Schematic of comparison of different RTM processes.
 - RTM
 - VARTM
 - RTM light
 - Compression RTM



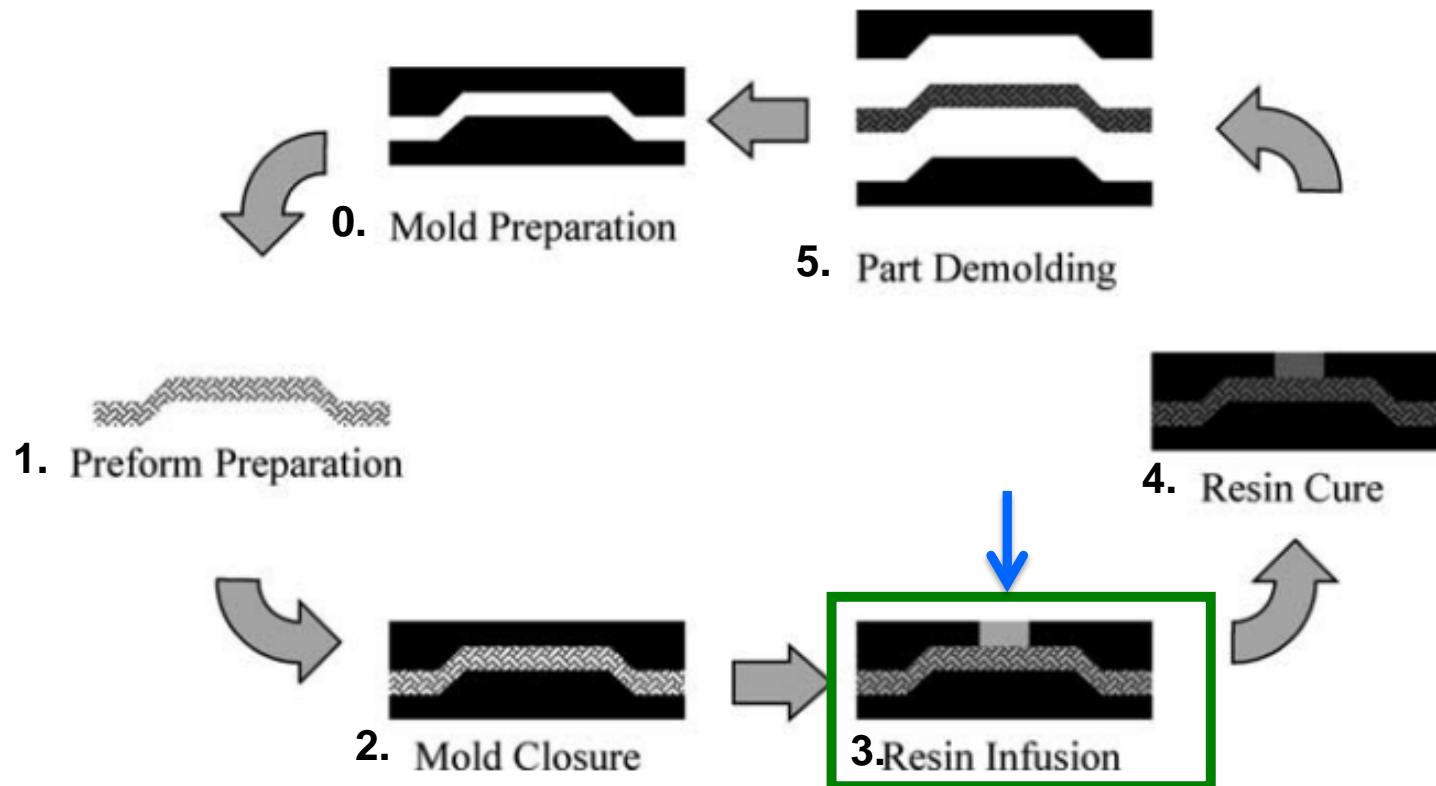
Pavel Simacek , SureshG. Advani, "Modeling resin flow and fiber tow saturation induced by distribution media collapse in VARTM", *Composites Science and Technology*, Volume 67, Issue 13, October 2007, Pages 2757–2769

Benefits and Disadvantages

Benefits	Disadvantages
<ul style="list-style-type: none">● Faster Production● Tight Dimensional Tolerance● Labor Savings● Repeatability● High surface finish● High mechanical performance	<ul style="list-style-type: none">● Mold design is complex● Higher Tool Cost● Requires leak-proof molds



Introduction RTM process steps



Source : A. Shojaei, S. R. Ghaffarian, S. M. H. Karimian, "Modeling and simulation approaches in the resin transfer molding process: A review", Polymer CompositesVolume 24, Issue 4, pages 525–544, August 2003

Issues and Objectives

> Issues

- The traditional simulation tools for RTM process use 2.5D model to analyze the filling behavior.
- These tools is not really suitable for simulating complex geometry and complex mat layers condition.

> Objectives

- To Simulate the resin Filling behavior through the novel 3D simulation technique.
- Compare the experiment and simulation result of actual manufacturing process

Implementation details

Governing Equation

> Continuity Equation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0$$

> The Equation of Energy

$$\frac{\partial}{\partial t}(\rho C_p T) + \nabla \cdot (\rho \mathbf{u} C_p T) = k \nabla^2 T + \eta \dot{\gamma}^2 + \phi \frac{d\alpha}{dt} \Delta H$$

> Darcy's Law

$$\mathbf{u} = -\frac{\mathbf{K}}{\eta} \nabla p$$

> Permeability Tensor

$$\mathbf{K} = \begin{bmatrix} K_{xx} & K_{xy} & K_{xz} \\ K_{yx} & K_{yy} & K_{yz} \\ K_{zx} & K_{zy} & K_{zz} \end{bmatrix}$$

ρ : fluid density

\mathbf{u} : velocity vector

\mathbf{K} : Permeability Tensor

T : temperature

t : time

p : pressure

η : viscosity

k : thermal conductivity

$\dot{\gamma}$: shear rate

C_p : specific heat

α : conversion

ΔH : Heat generation of reaction

Viscosity and Kinetic Model

- > Curing kinetic model:
 - Combined model

$$\frac{d\alpha}{dt} + \mathbf{u} \cdot \nabla \alpha = (K_a + K_b \cdot \alpha^m) (1 - \alpha)^n$$

- > Viscosity model:
 - Cross Castro-Macosko model

$$\eta = \frac{\eta_0 \left(\frac{\alpha_g}{\alpha_g - \alpha} \right)^{c1+c2\alpha}}{1 + \left(\frac{\eta_0 \cdot \dot{\gamma}}{\tau^*} \right)^{1-n}}$$

$$\eta_0 = A \exp\left(\frac{T_b}{T}\right)$$

η : viscosity

η_0 : zero shear rate viscosity

α : conversion

n : the power law index

$\dot{\gamma}$: shear rate

α_g : conversion the gel point,

T : temperature

\mathbf{u} : velocity vector

K_a, K_b : material constants

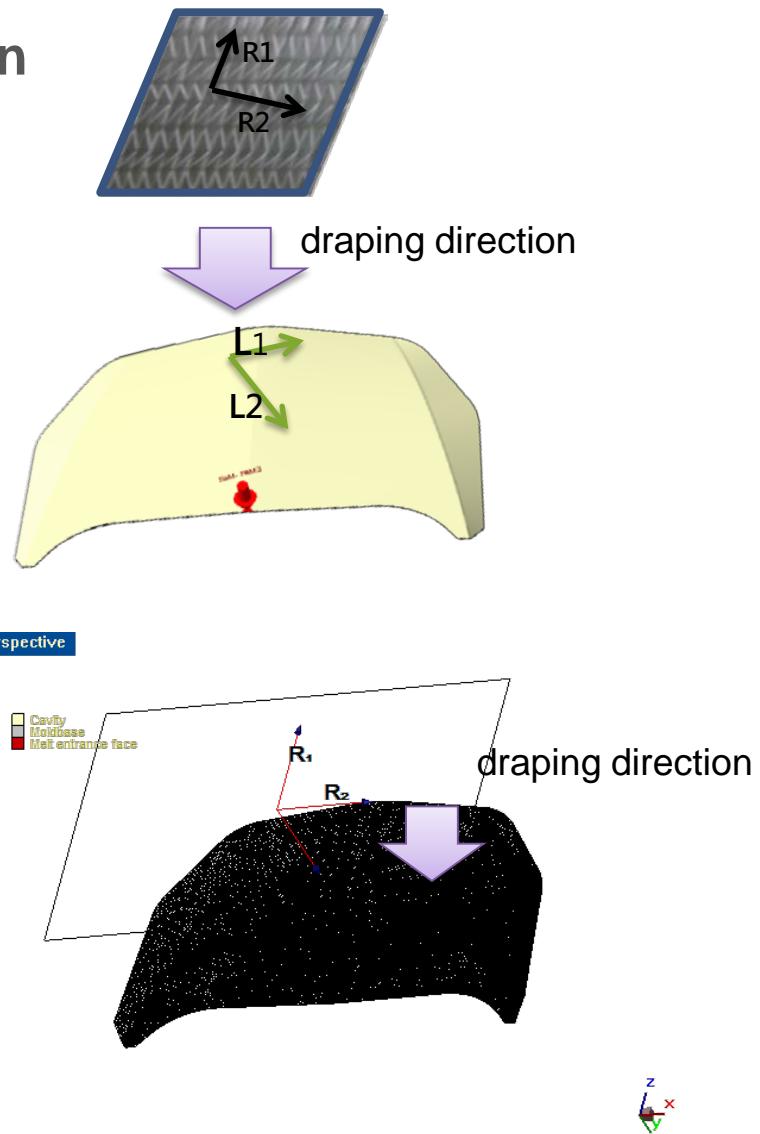
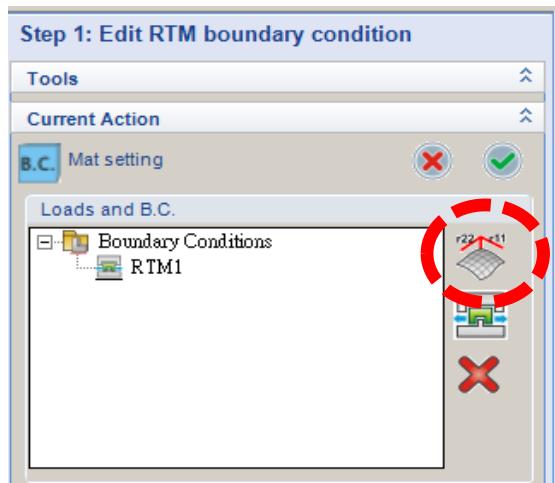
t : time

Mat Orientation of Fiber Preform

> Permeability tensor axis direction

– Fiber mat orientation

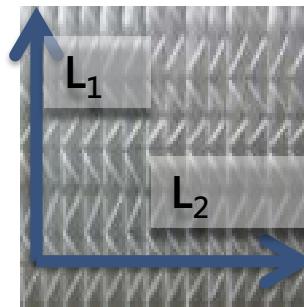
- Before draping \vec{R}_1, \vec{R}_2
- After draping \vec{L}_1, \vec{L}_2



Set Permeability tensor

> Permeability tensor axis direction

$R_x = (1.0, 0.0, 0.0)$
 $R_z = (0.0, 1.0, 0.0)$



$$\mathbf{L}_1 = (l_{11}, l_{12}, l_{13})$$
$$\mathbf{L}_2 = (l_{21}, l_{22}, l_{23})$$
$$\mathbf{L}_3 = (l_{31}, l_{32}, l_{33})$$

Fiber mat orientation Before draping

K_{11} cm^2
 K_{22} cm^2
 K_{33} cm^2
porosity

$$\mathbf{K} = \begin{bmatrix} K_{xx} & K_{xy} & K_{xz} \\ K_{yx} & K_{yy} & K_{yz} \\ K_{zx} & K_{zy} & K_{zz} \end{bmatrix}$$
$$= \begin{bmatrix} l_{11} & l_{12} & l_{13} \\ l_{21} & l_{22} & l_{23} \\ l_{31} & l_{32} & l_{33} \end{bmatrix} \begin{bmatrix} K_{11} & 0 & 0 \\ 0 & K_{22} & 0 \\ 0 & 0 & K_{33} \end{bmatrix} \begin{bmatrix} l_{11} & l_{21} & l_{31} \\ l_{12} & l_{22} & l_{32} \\ l_{13} & l_{23} & l_{33} \end{bmatrix}$$

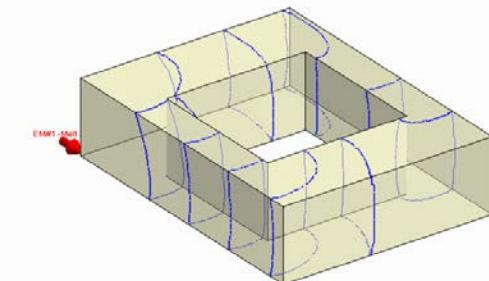
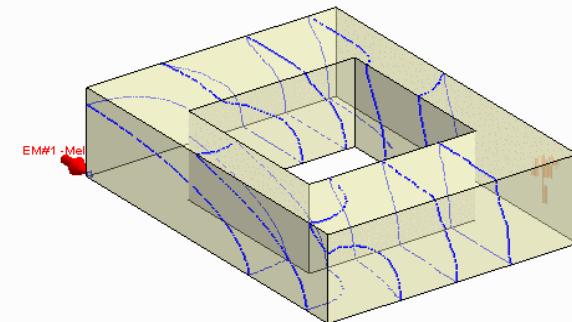
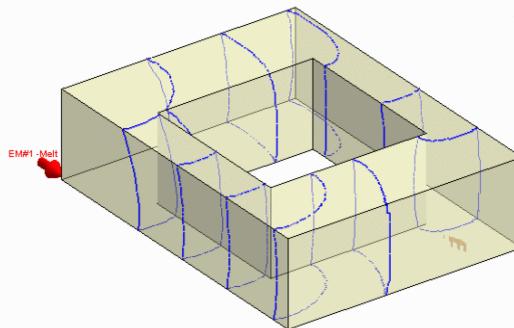
Set Permeability tensor principal value

Anisotropic Permeability Tensor (principal value)

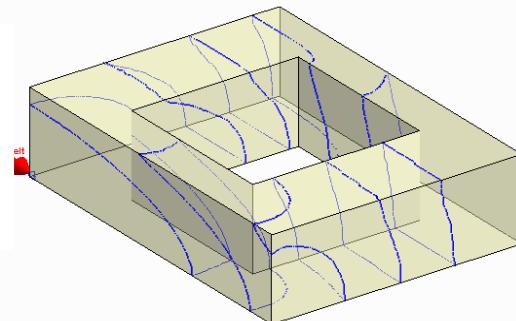
- > Compare with result between Isotropic and Anisotropic permeability

$$\mathbf{K} = \begin{bmatrix} K_{xx} & K_{xy} & K_{xz} \\ K_{yx} & K_{yy} & K_{yz} \\ K_{zx} & K_{zy} & K_{zz} \end{bmatrix} = \begin{bmatrix} K_{11} & 0 & 0 \\ 0 & K_{22} & 0 \\ 0 & 0 & K_{33} \end{bmatrix} = \begin{bmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 1 \end{bmatrix}$$

$$\mathbf{K} = \begin{bmatrix} K_{xx} & K_{xy} & K_{xz} \\ K_{yx} & K_{yy} & K_{yz} \\ K_{zx} & K_{zy} & K_{zz} \end{bmatrix} = \begin{bmatrix} K_{11} & 0 & 0 \\ 0 & K_{22} & 0 \\ 0 & 0 & K_{33} \end{bmatrix} = \begin{bmatrix} 10 & 0 & 0 \\ 0 & 2.5 & 0 \\ 0 & 0 & 1 \end{bmatrix}$$



Isotropic permeability
 $K_{11} : K_{22} : K_{33} = 1:1:1$



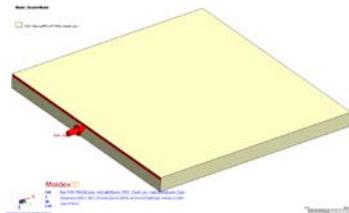
Anisotropic permeability
 $K_{11} : K_{22} : K_{33} = 10:2.5:1$

Multi-layer fabric preforms

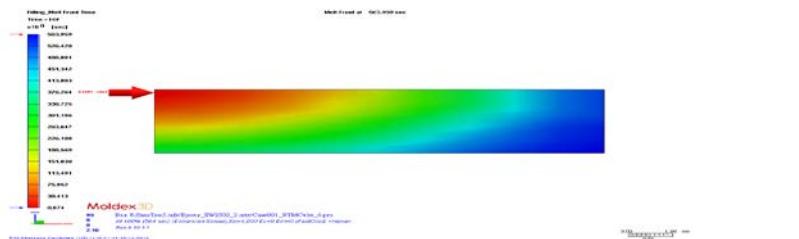
- > Support to assign different Permeability for different regions

Distribution Media

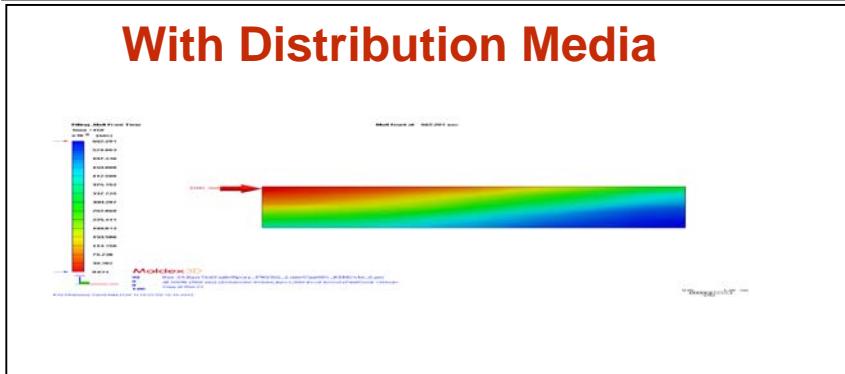
Fiber Mat



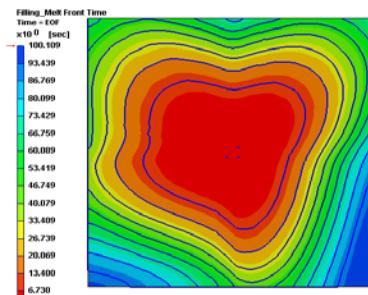
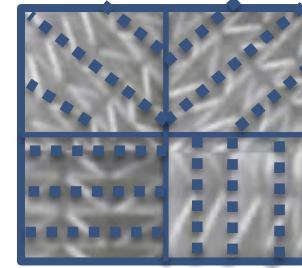
Without Distribution Media



With Distribution Media

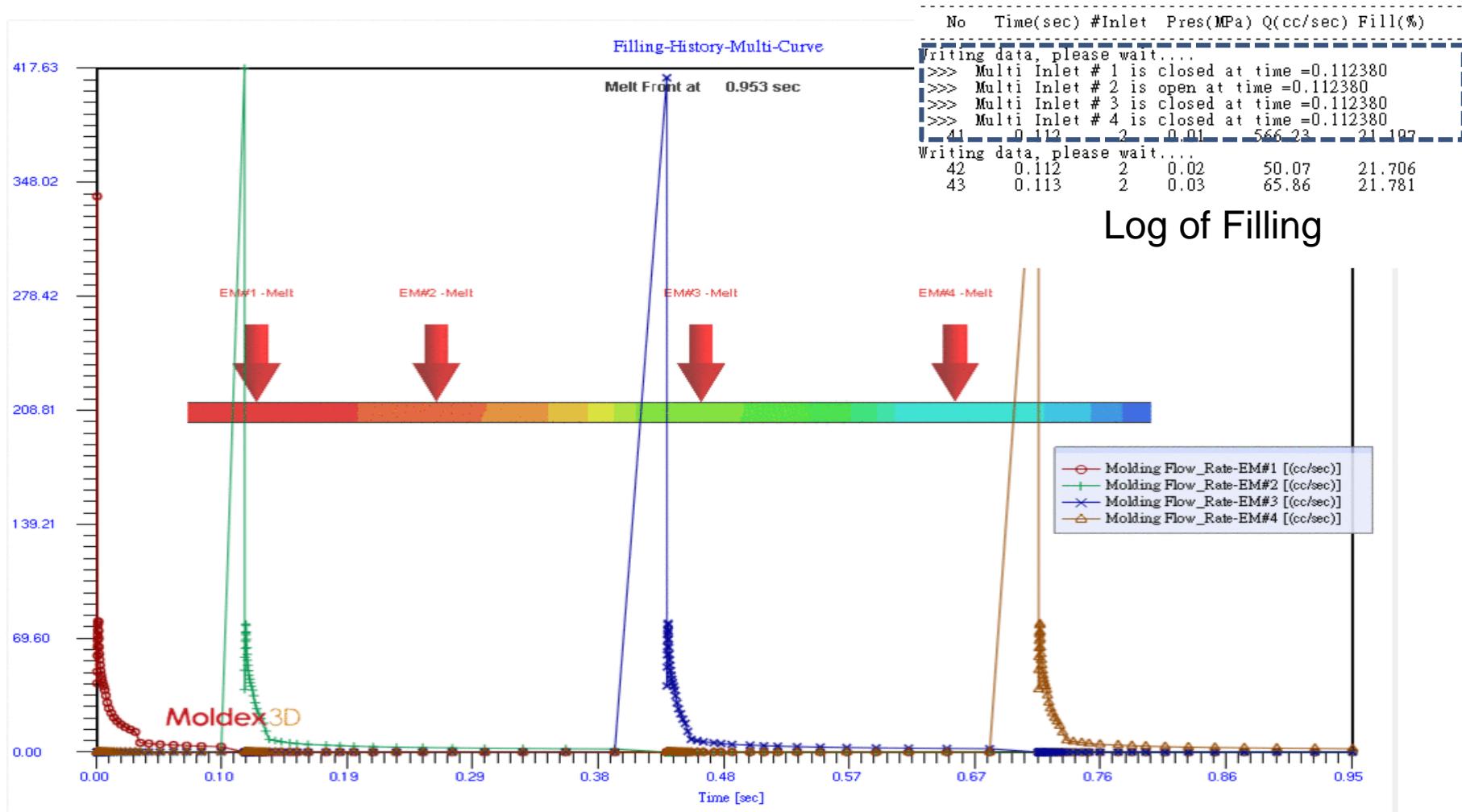


Orientation of fiber preforms affect filling behavior



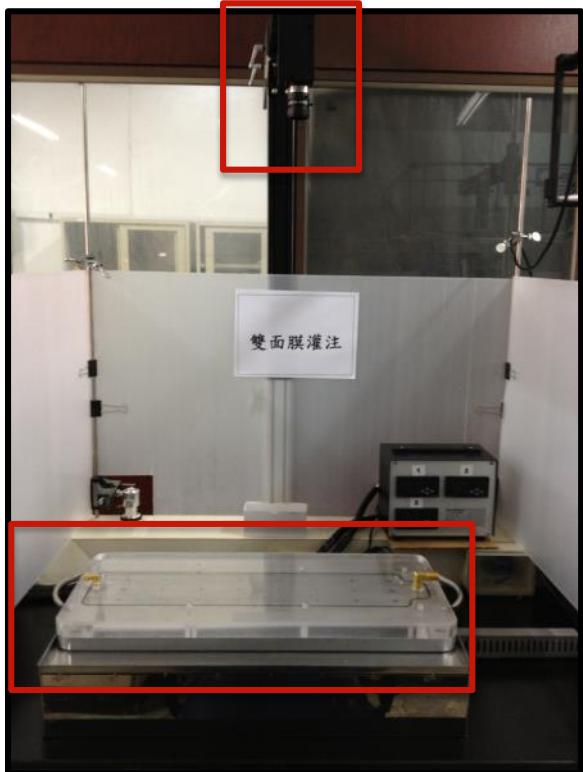
Multi-Inlet Control

> Multi-inlet Open/Close period control by sensor nodes

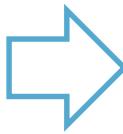


Permeability Measurement

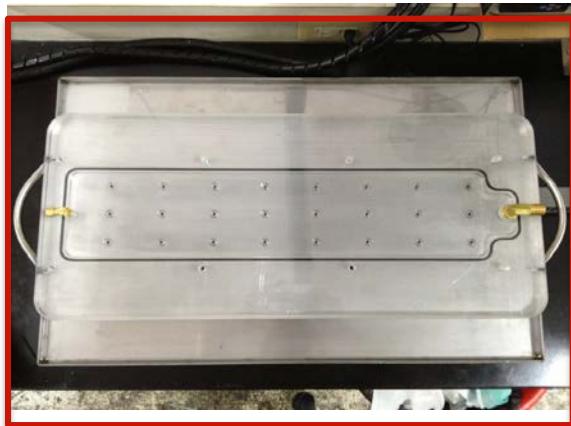
Visualization system



Camera



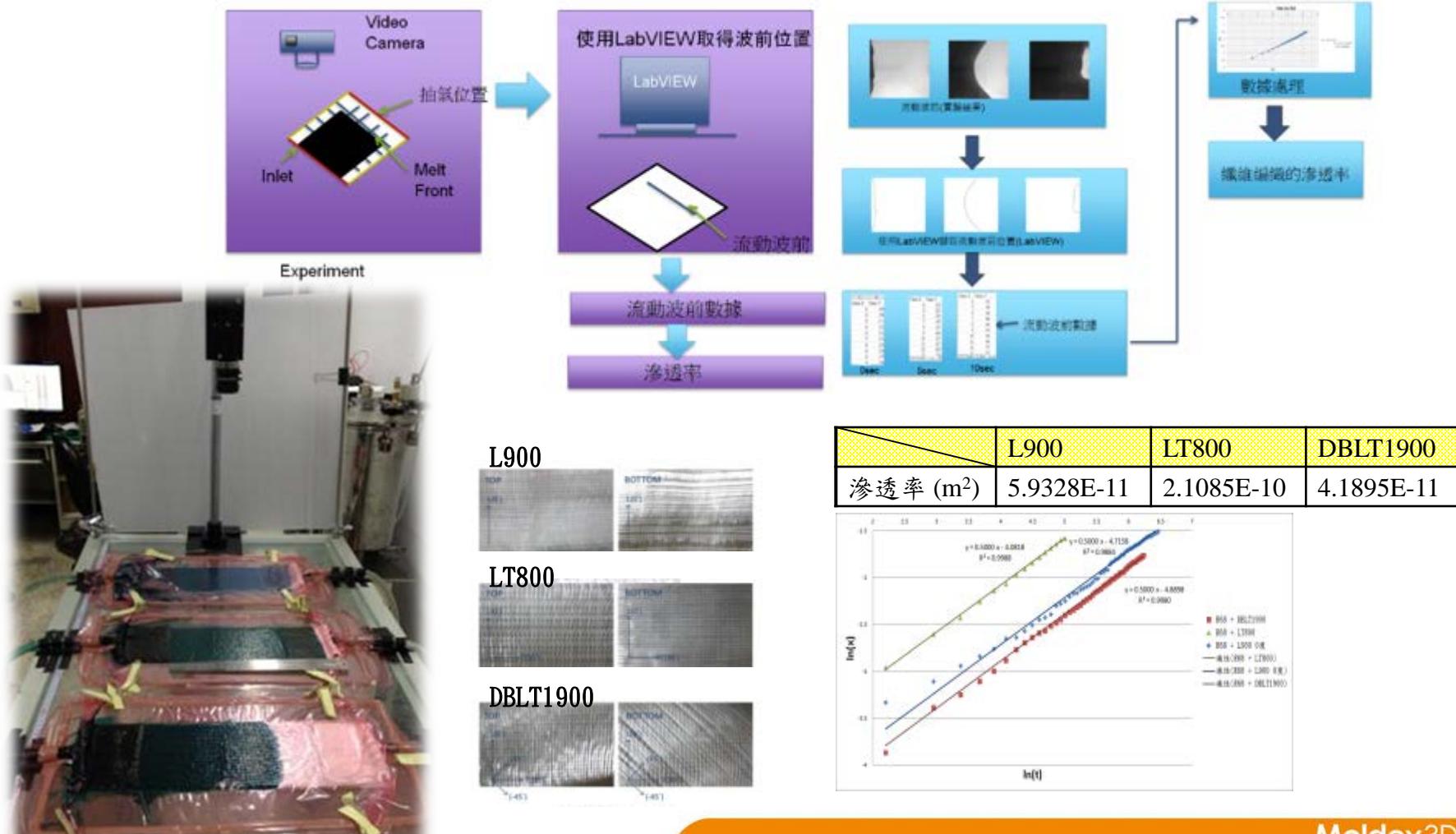
Mold



Visualization system

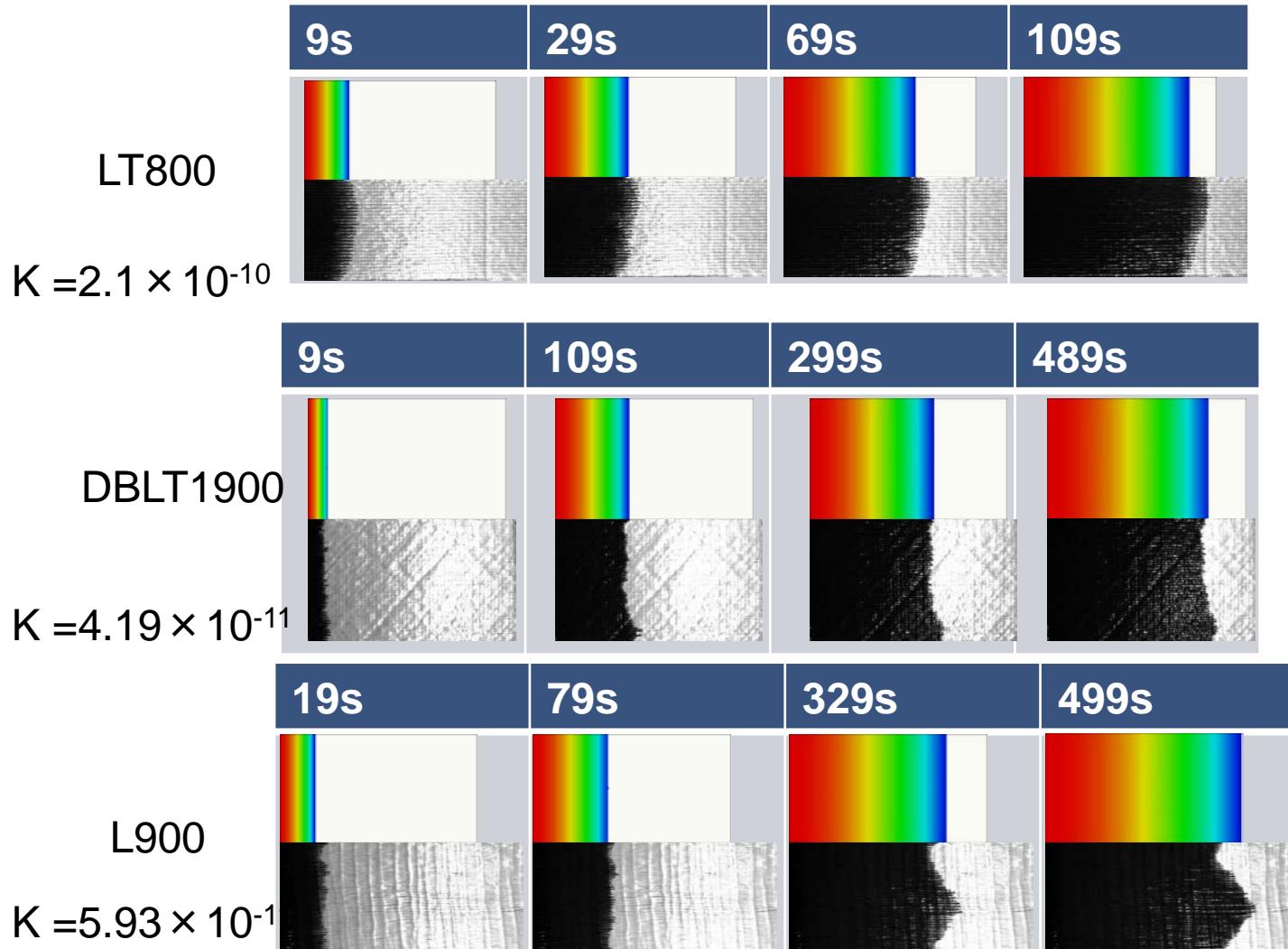
Integrated system for permeability measurement

- > A integrated system to transfer the melt front during filling process to get the permeability by Darcy's law



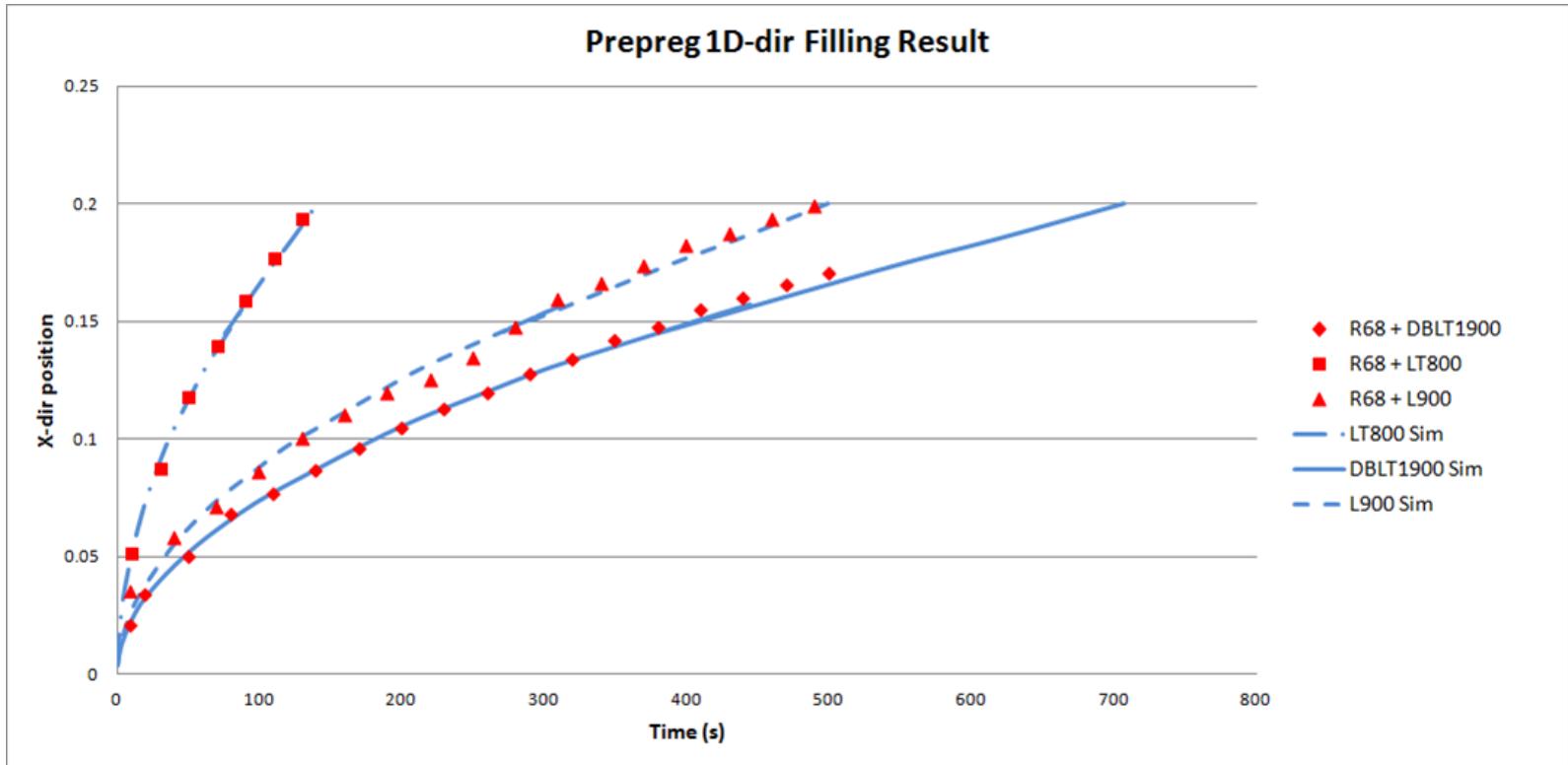
Permeability Measurement Result

> Compare with different fiber mats



Result

- > Experiment compare with the RTM Simulation



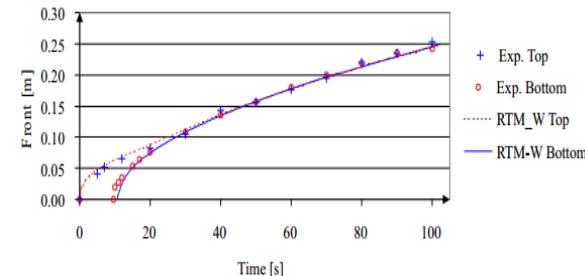
2-D Simulation

Case 1 Single material preforms CFM 450

Case 1 : Single material preforms

Reference Study

- > Fabric preform:
 - CFM 450
- > Single component of fabric preform
 - Viscosity = 0.239 Pa s
- > Operating Condition
 - Inlet Pressure = 0.9 atm = 0.09 MPa



K and ϕ	K_{11} (m ²)	K_{22} (m ²)	K_{33} (m ²)	ϕ (-)
CFM 450	1.04E-9	1.04E-9	5.16E-10	0.8

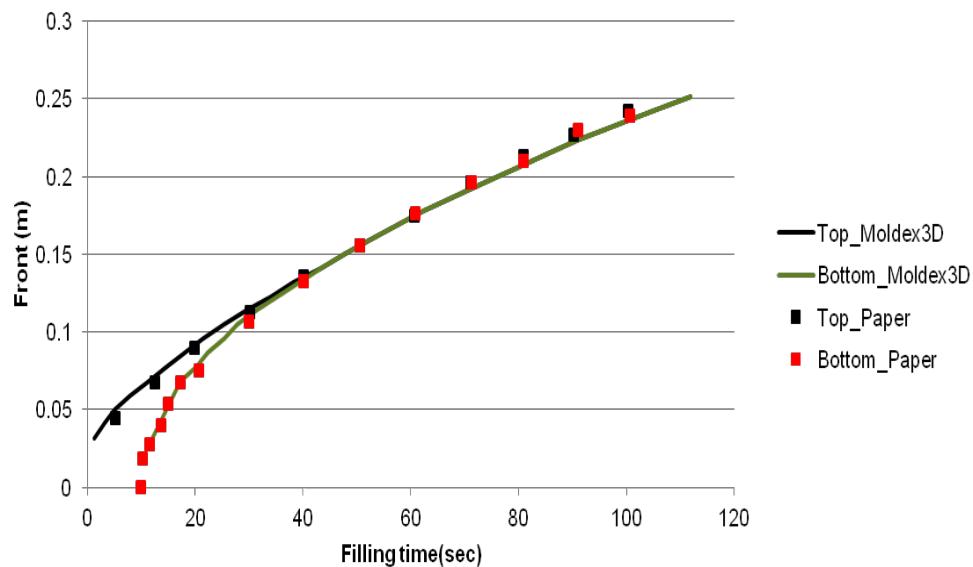
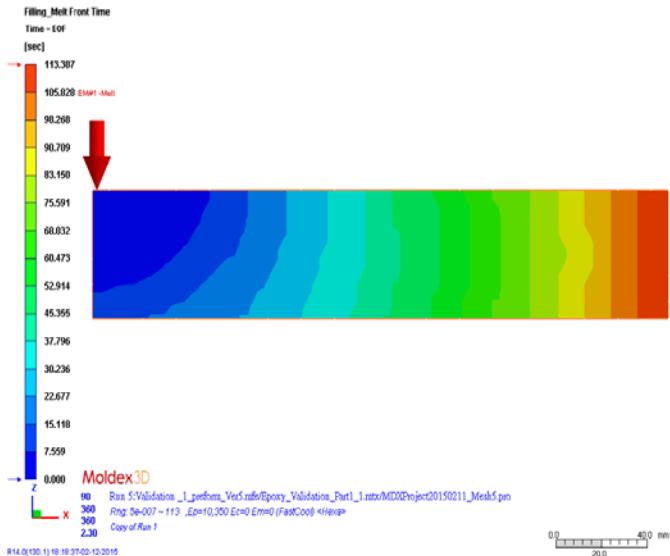


Figure 7.8: CFM450 50 layers lay-up.

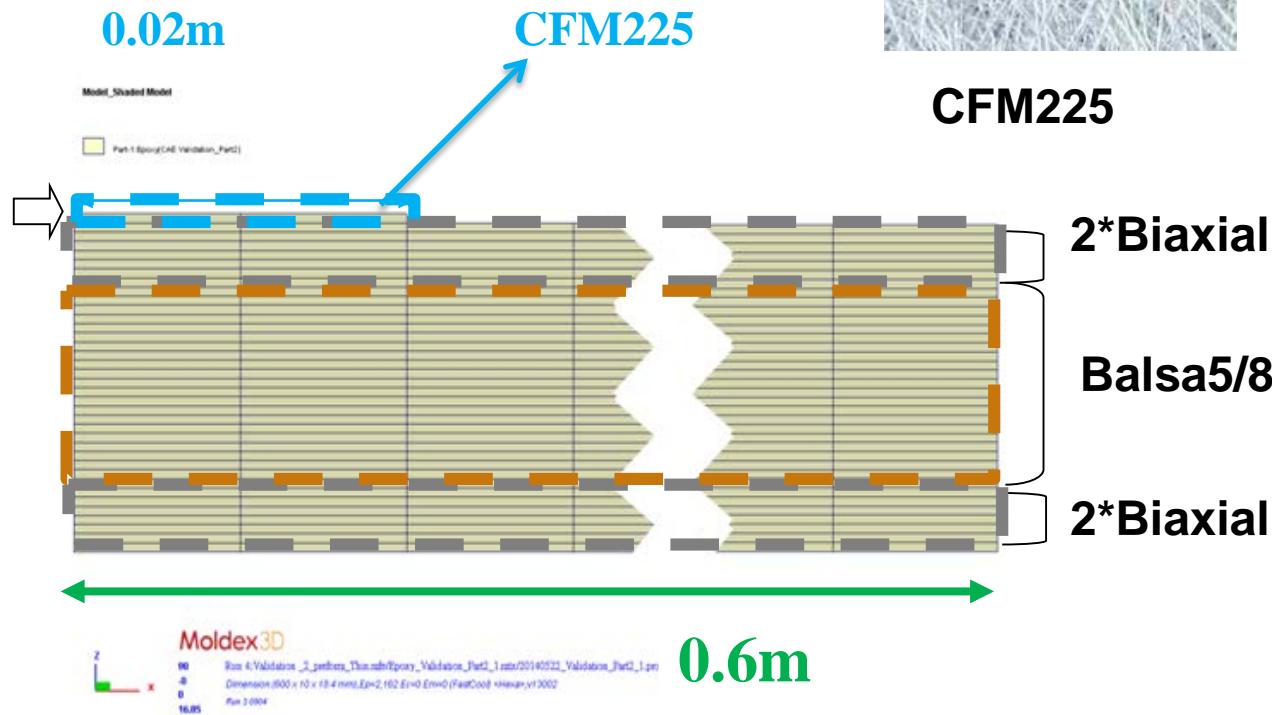
Reference : Koefoed, M. "Modeling and simulation of the VARTM Process for Wind Turbine Blades." *Industrial Ph. D. Dissertation* (2003).

Moldex3D RTM Simulation Result

- > Flow front time result at end of filling stage and flow front location vs. filling time.



Case 2 : Sandwich Structure Geometry and Fabric Preforms



Biaxial Fib



Balsa5/8

Picture Reference

1. <http://nuplex.com/Composites/products/browse-products/corematerials/gurit%E2%84%A2-balsaflex>
2. <http://www.ec21.com/product-details/Fiberglass-Biaxial-0-90-Degree--7506537.html>
3. http://www.alibaba.com/product-detail/Glass-Fiber-Continuous-Filament-Strand-Mat_327073845.html

Material Property and Operating condition

> Material Property

- Viscosity = 0.239 Pa s

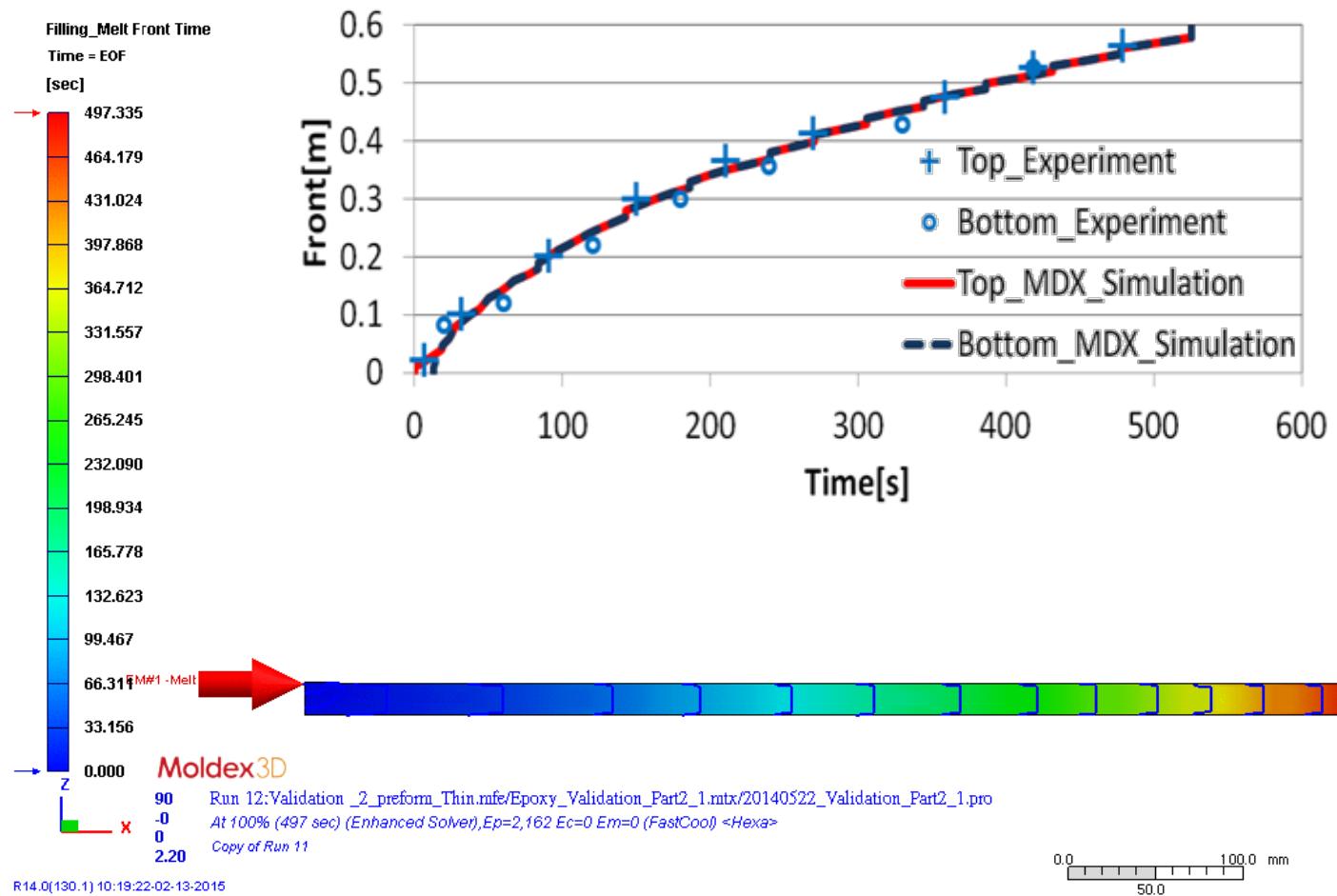
K and ϕ	K_{11} (m ²)	K_{22} (m ²)	K_{33} (m ²)	ϕ (-)
CFM225	1.16E-9	1.16E-9	5.44E-10	0.81
Biaxial	1.8E-13	1.8E-13	1.11E-12	0.44
Balsa 5/8	4.4E-11	1.47E-10	1.47E-10	0.11

> Operating Condition

- Inlet Pressure = 0.9 atm = 0.09 MPa

Moldex3D RTM Simulation Result

> Flow front animation and front location vs. filling time.



3-D Simulation

3D flow behavior prediction in RTM

Background (1)

- > Industrial challenge
 - How to make the smooth filling for huge part?
 - What is the filling behavior

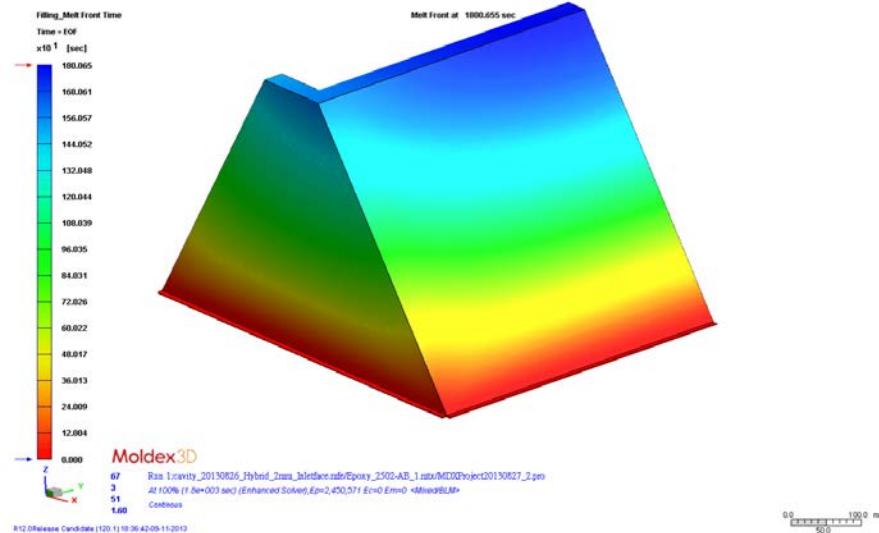
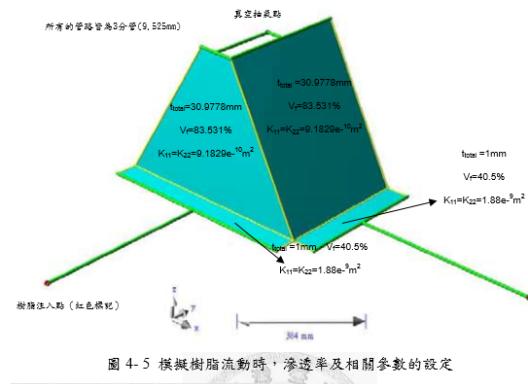


圖 4-2 模型焊道突出示意圖



Background (2)

- > Reference
 - Study on the application of VARTM technique and mold flow analysis to the lamination of sandwich plates
- > Professor
 - Ya-Lung Lee
- > Author
 - Kai-Lin Chen
- > Polymer
 - Eternal Chemical 1629
 - Environment temperature 24.4°C
 - D+P+(MR)*1+M+DC+(MR)*1+M
 - D: distribution media
 - P: peel ply
 - M: fiber mat
 - DC: double cut core



Geometrical System

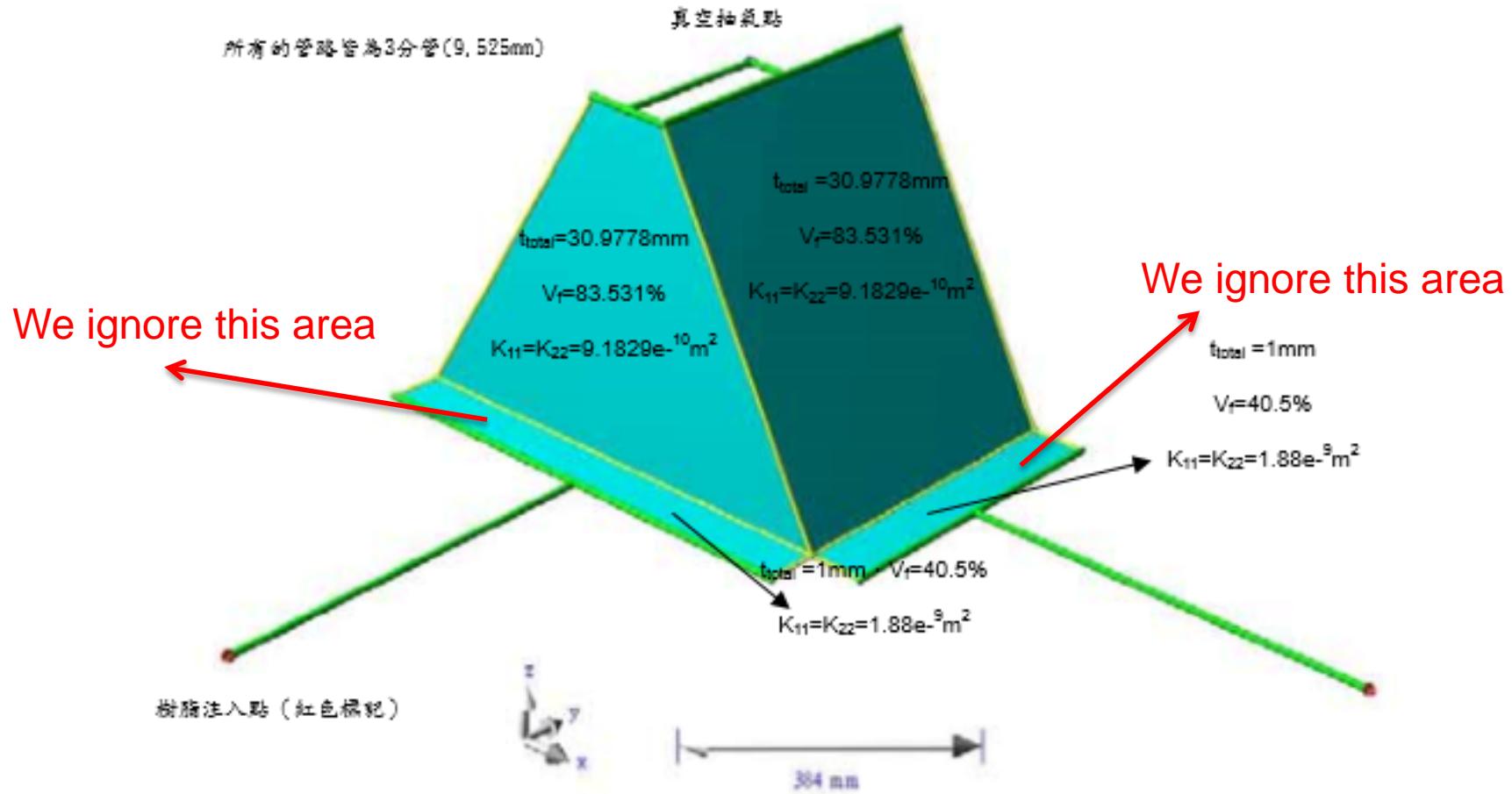
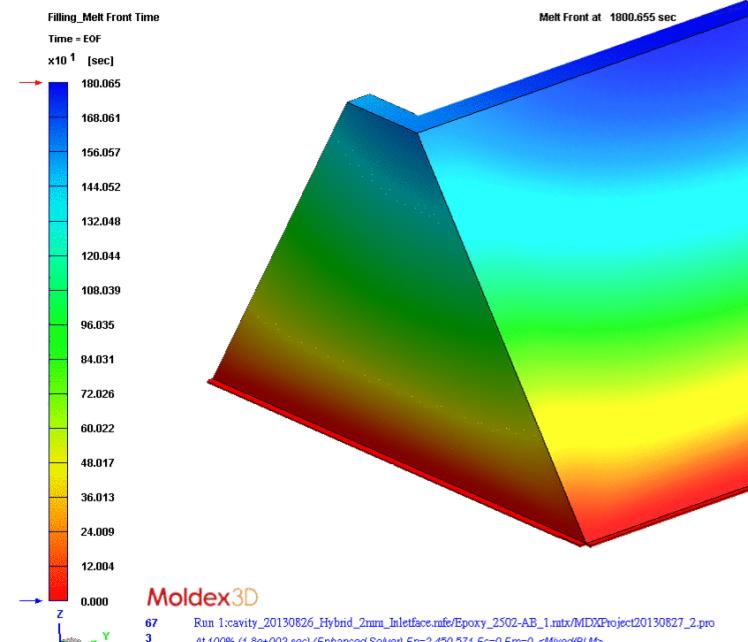


圖 4-5 模擬樹脂流動時，滲透率及相關參數的設定

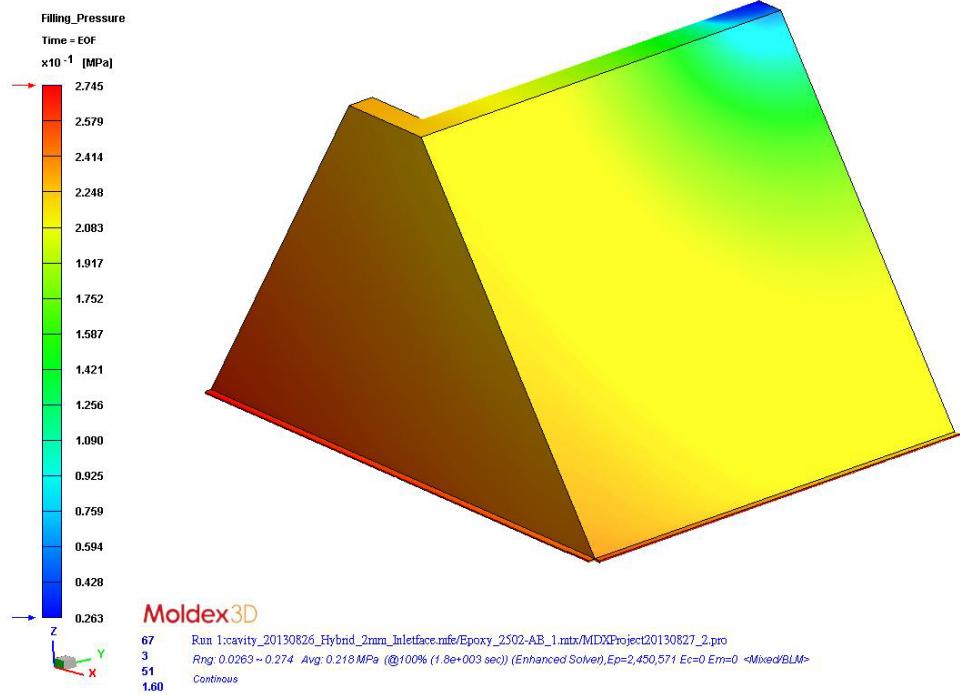
Reference : Study on the application of VARTM technique and mold flow analysis to the lamination of sandwich plates

Filling Results: $Q=6.35 \times 10^{-6} \text{m}^3$

Melt Front Time



Pressure Distribution



Comparison with Research (1/2)



圖 4-6 樹脂灌注實驗與模擬流動圖形比較圖(矩形面)

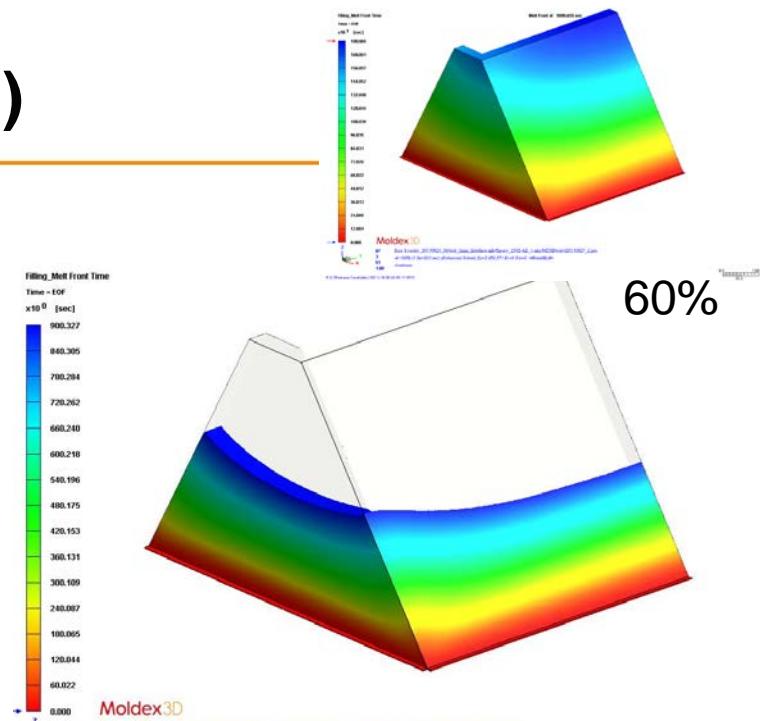
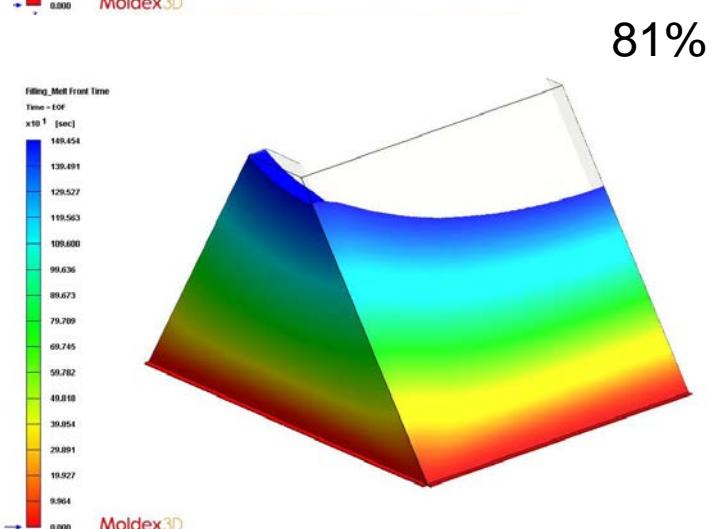
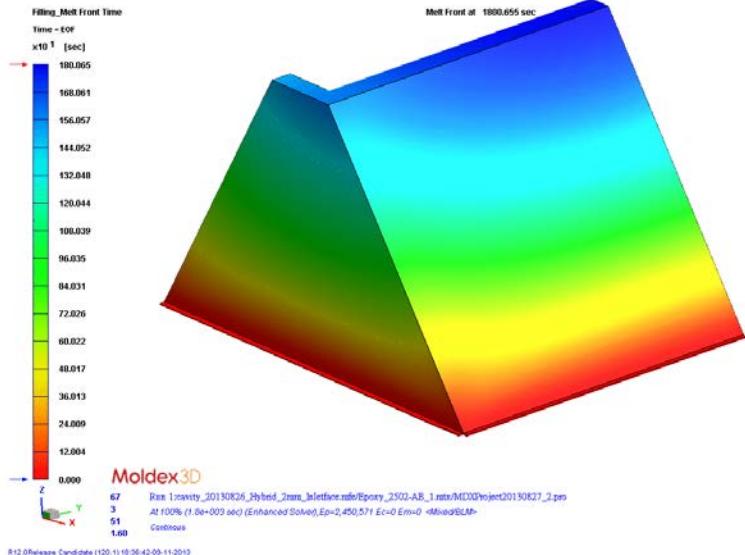


圖 4-7 樹脂灌注實驗與模擬流動圖形比較圖(梯形面)

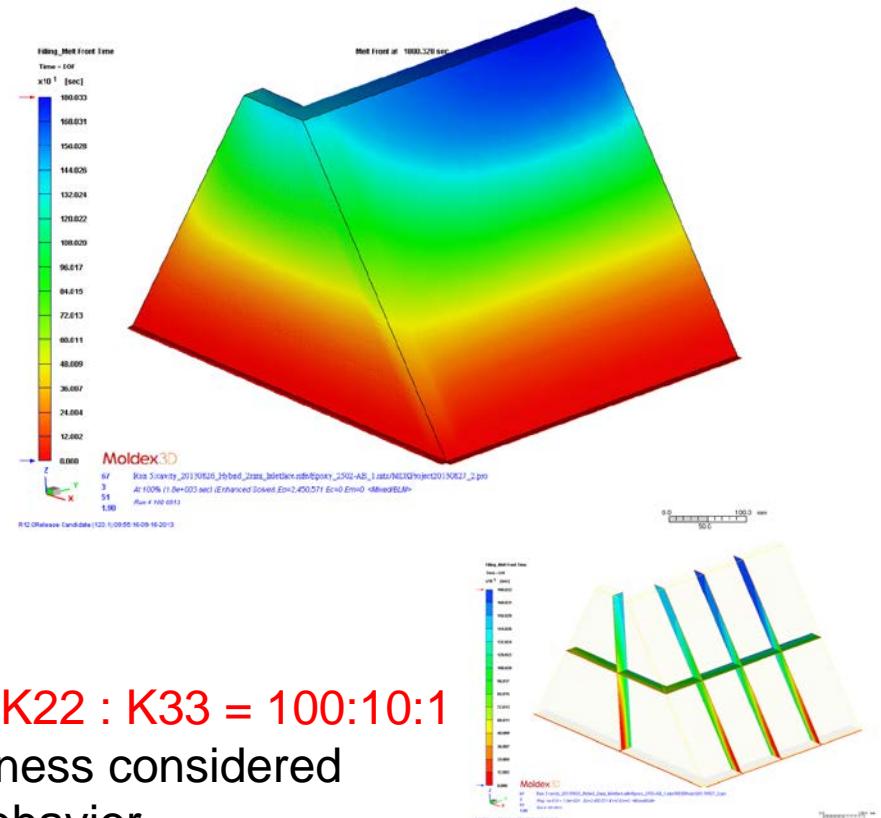


Reference :Study on the application of VARTM technique and mold flow analysis to the lamination of sandwich plates

Adding the Thickness Effect



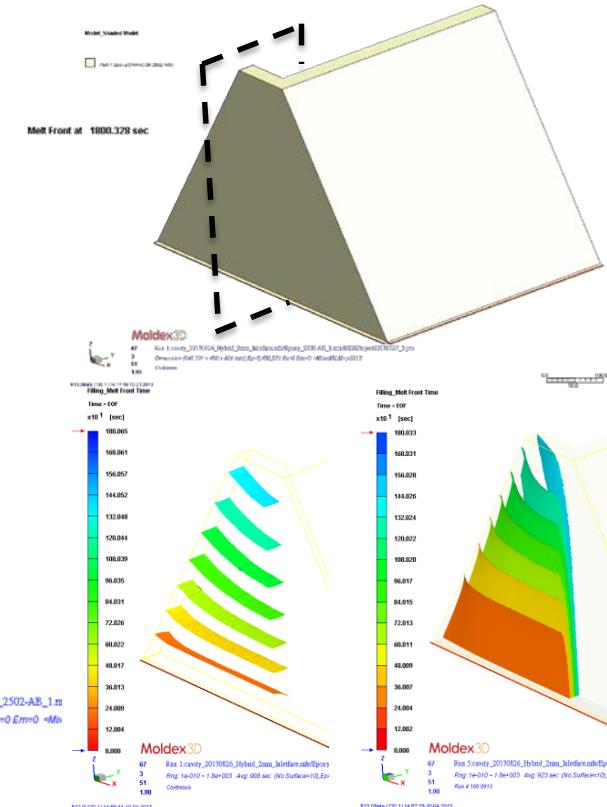
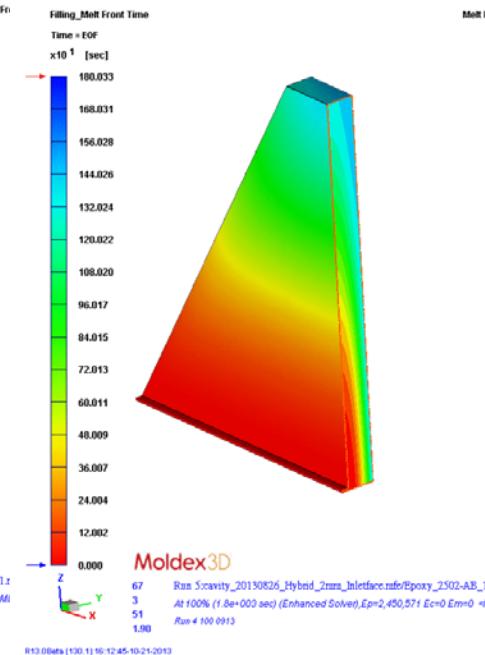
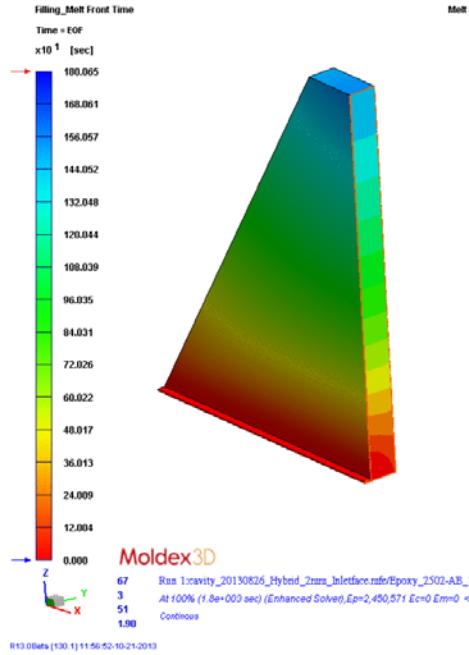
K11 : K22 : K33 = 1 : 1 : 1
Thickness not considered
2D Behavior



K11 : K22 : K33 = 100:10:1
Thickness considered
3D Behavior

Melt Front Difference Across the Thickness

Capturing the thickness difference with a true 3D simulation



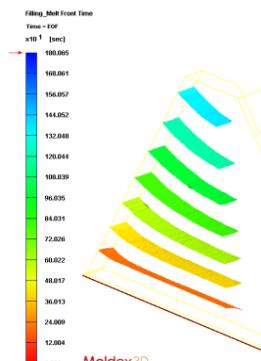
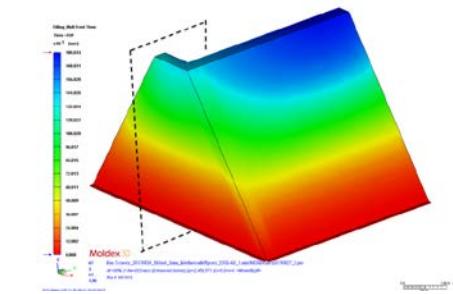
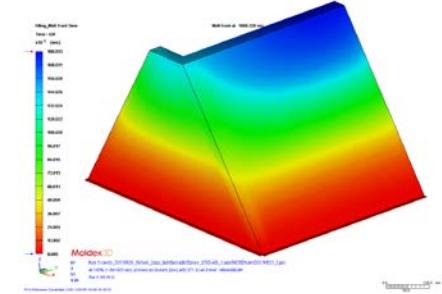
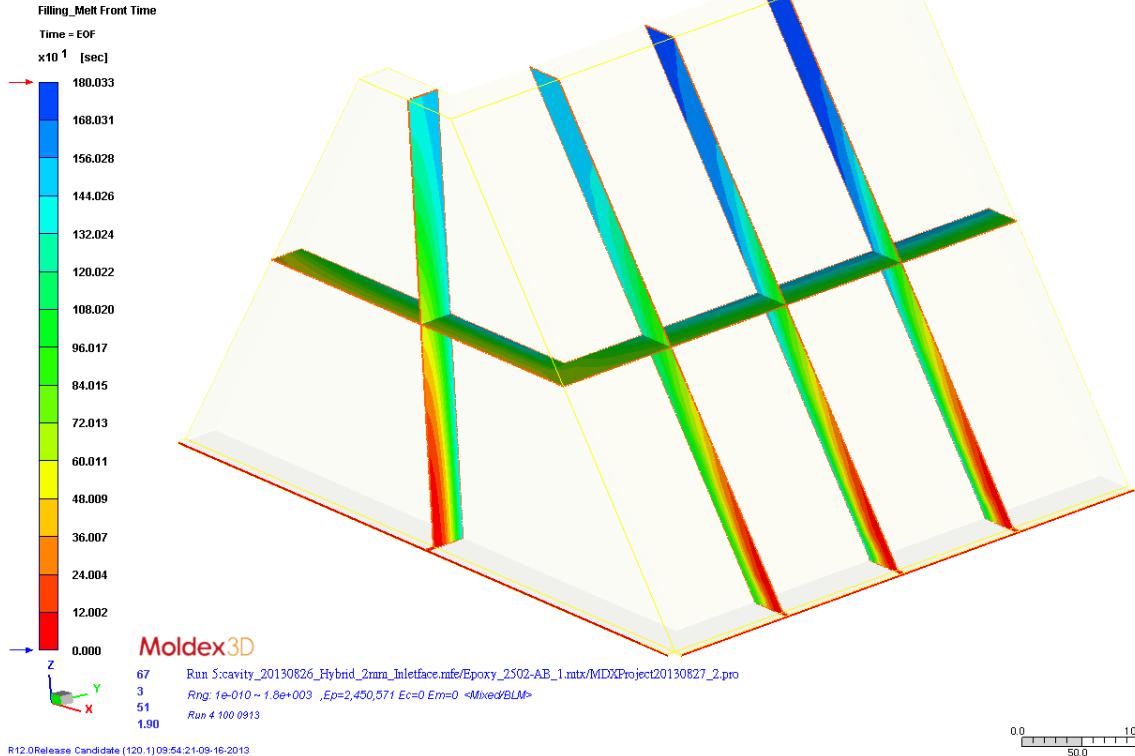
Isotropic

Anisotropic

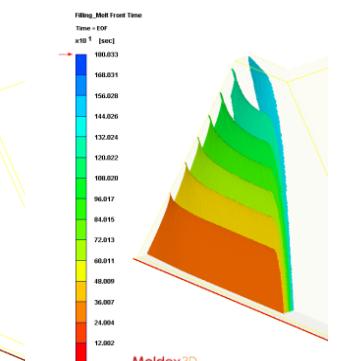
Isotropic

Anisotropic

Melt Front Difference Across the Thickness



Isotropic



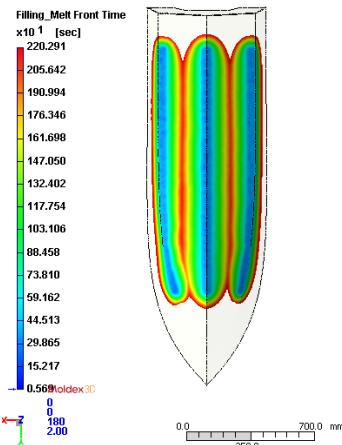
Anisotropic

3-D Simulation

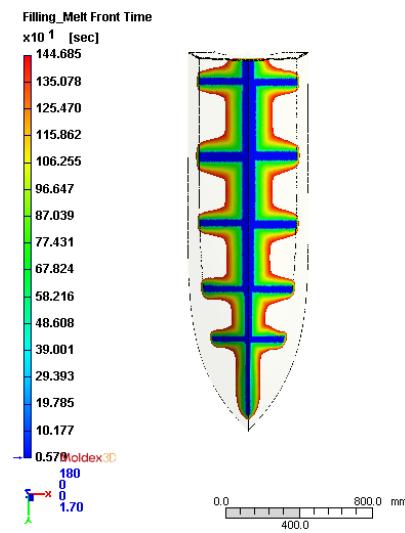
Boat

Case 1: 改變佈管形式對於船殼灌注

> 改變佈管形式



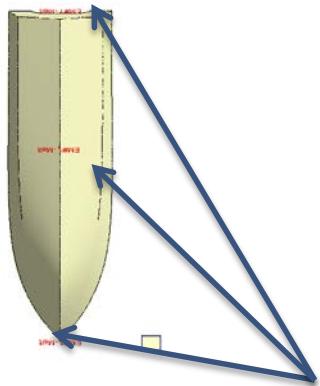
Experiment result



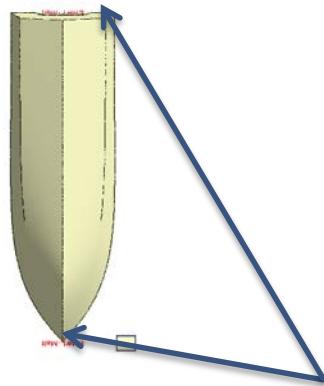
Simulation result

不同的佈管形式

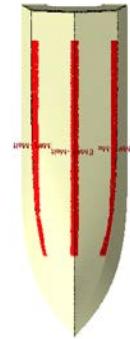
> 以模擬方式評估佈管方式



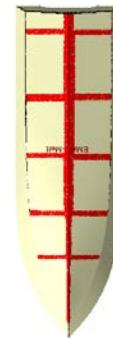
三進澆口方式



兩進澆口方式



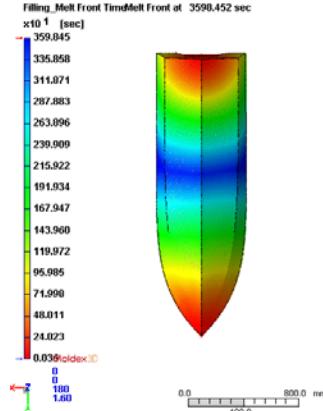
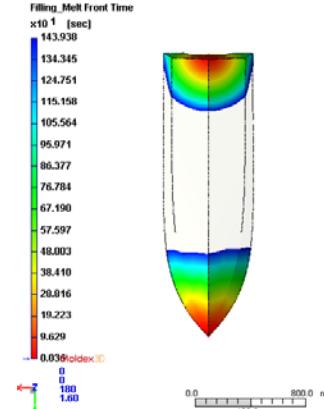
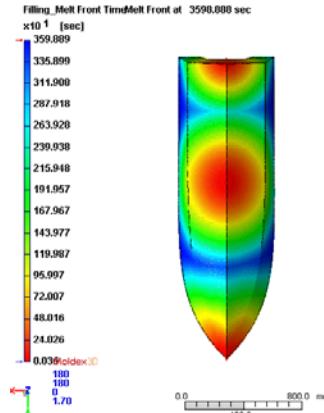
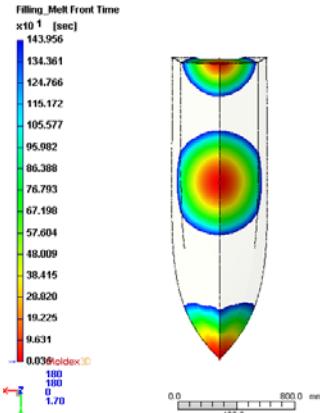
平行型佈管



魚骨型佈管

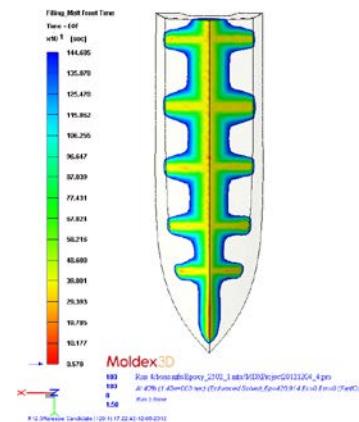
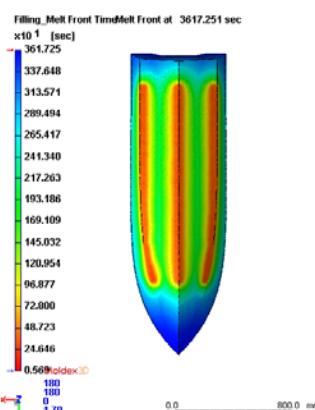
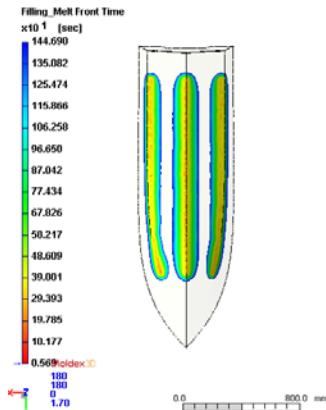
流動波前結果

> 比較各種進澆的方式



三進澆口方式

兩進澆口方式

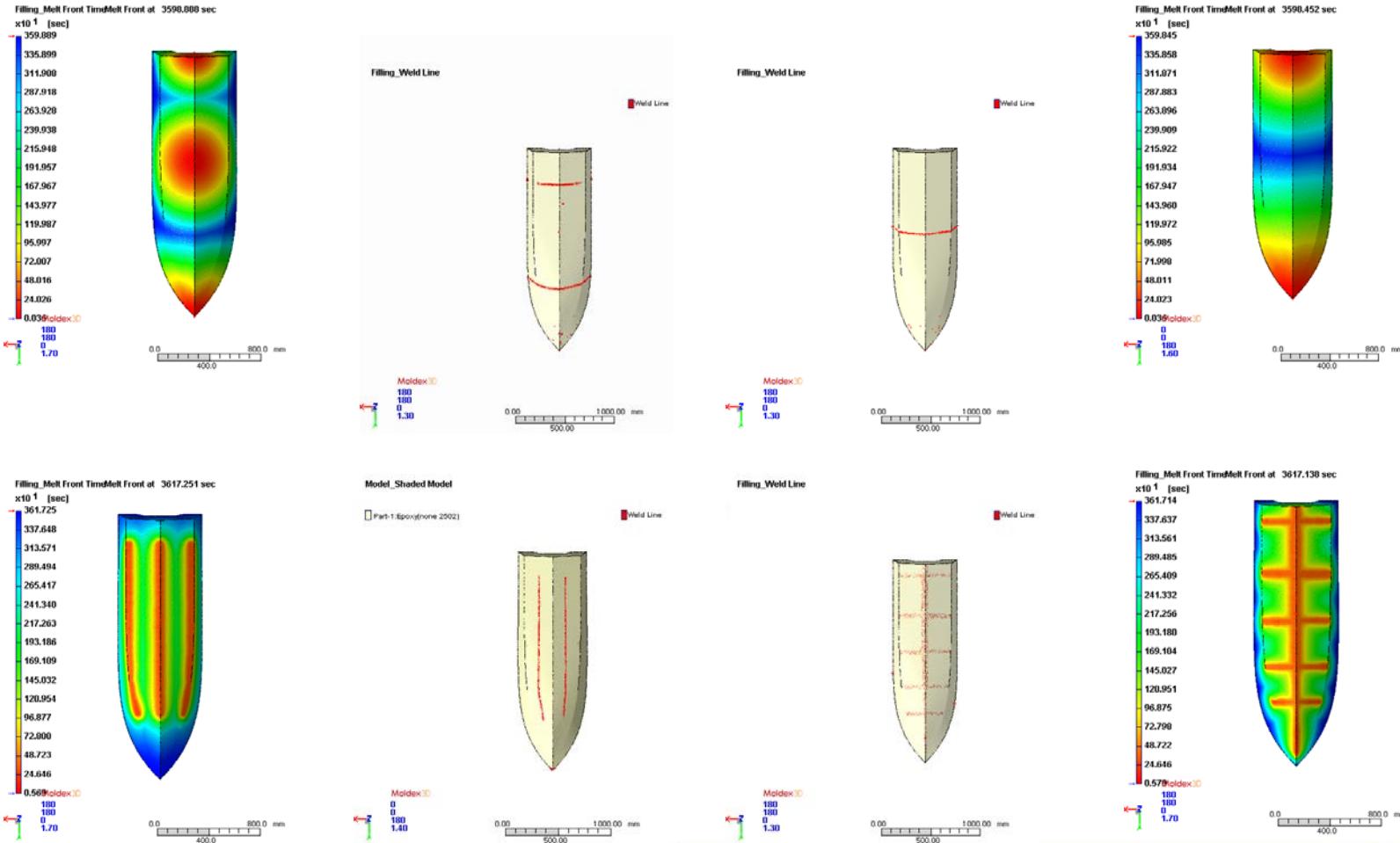


平行型佈管

魚骨型佈管

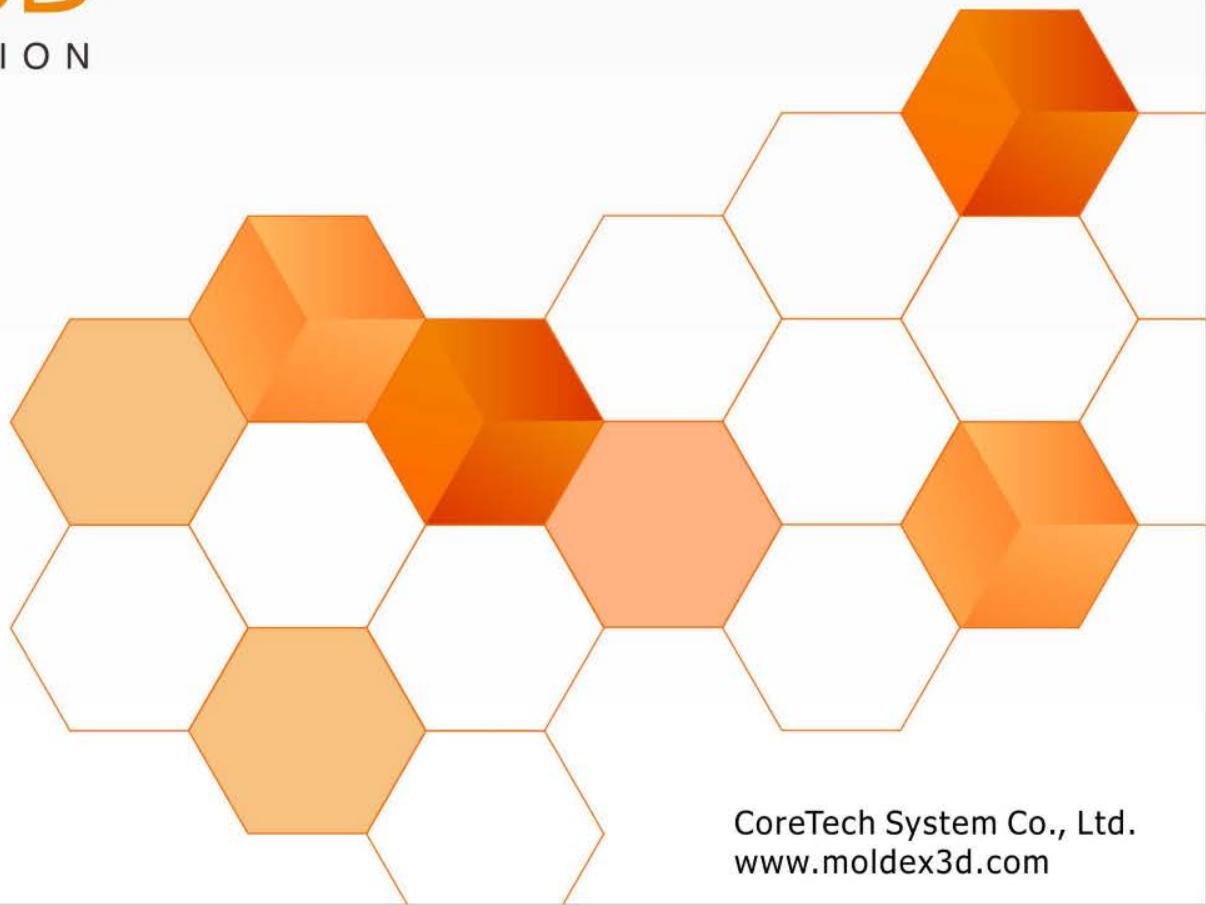
波前交會線

> 不同佈管方式下波前交會造成波前交會線



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